

Case study

Purity Brewing Co., near Alcester, West Midlands

Since 2005 Purity Brewing Co, based near Alcester in the West Midlands, has been using a passive wetland system, designed by Cress Water Solutions, to treat the wastewater from their brewing operations. At that time they were just starting up in converted farm buildings. Fortunately the farmer had plenty of land available all sloping away from the farm buildings making it possible to design a wetland system driven entirely by gravity. Originally it was designed for a maximum wastewater discharge of 10 m³/day. Following the success of this multi-award winning brewery, production has more than doubled and the system has had to be redesigned and enlarged to cater for up to 45 m³ of wastewater per day.



Previous experience had shown us that brewery wastewater is much stronger than is generally thought. Accordingly before starting we carried out a composite sampling programme at a similar sized working brewery to provide a reasonable basis on which to design the wetland system. We found BOD₅ levels varied daily from 1,800 mg/l to 7,270 mg/litre with an average value of 3,878 mg/l.



From experience with other breweries and results from this one we find the initial BOD₅ levels of the wastewater effluent are generally 4,000 - 7,000 mg/litre, 20-30 times stronger than domestic sewage.

To begin with the wastewater from the brewery is sieved to remove gross solids before passing into a large septic tank, that also takes the foul water from the staff toilets, where further settlement of solids takes place.

As the effluent at this stage is quite strongly acidic pH neutralisation is achieved by adding lime.

In the original system the effluent from the septic tank flowed into a anaerobic pond which, at a maximum design flow had an hydraulic retention time of 20 days. Here mixing took place. From there it passed into a wetland system comprised of two broad, long parallel swale ditches dug along contour lines. Soil excavated from the ditches was placed on the downhill sides of the ditches forming low banks which were densely planted with willows. Effluent passing through the soil matrix of the banks and past the network of willow tree roots is collected in a "chinampa ditch" which leads the partially treated effluent downhill to a ditch adjacent to the first of two large oxidation ponds. The second pond has a large horizontal flow reed-bed at its distal end.

Both ponds are planted extensively with a variety of marginal pond plants. The system discharges to a field ditch with running water in it.

The only part of the system that is lined is the anaerobic pond.

Effluent moves from one part of the system to the next solely by percolation through the surface soil layers, overflow and passage past the roots of the willow trees and through grasses and other vegetation that has grown up naturally.



In October 2009 we were asked to assess the system with regards to its capacity to handle a much larger loading when production at the brewery was being planned to be substantially increased. This gave us the first opportunity to take samples throughout the system and assess its performance. Samples were taken from the anaerobic pond, both swales, the chinampa ditch and from each of the two ponds.



Water levels in both ponds were low and there was no discharge from the system. The samples from the two ponds were, therefore, taken from the distal ends of the bodies of water in them. The results are presented in Table 1 below.

We were excited and pleased to find from these results that the simple wetland system installed to treat a rather strong brewery effluent was performing extremely well 4 years after its installation. At that time it was achieving a BOD5 reduction of better than

99.94%, an ammonia reduction of 98.26% and a phosphate reduction of 94%.

Table 1. Results of analyses of samples taken from a wetland system serving a small brewery 4 years after installation.

Sampling Location	pH	BOD5	COD	SS	Ammonia	TON	Phosphate	Chloride
		mg/l	mg/l	mg/l	mg/l	mg/l	mg/l	mg/l
Anaerobic Pond	4.55	5690	8960	224	34.4	3.74	51.4	60.8
Swale Ditch 1	5.49	2780	4480	194	77	<1.00	49.6	64.2
Swale Ditch 2	7.40	665	1630	167	68.5	<1.00	42.8	62.7
Chinampa Ditch	7.88	23.2	234	66	44.6	<1.00	24	59.4
Pond 1	8.11	4.45	149	17	11.5	<1.00	6.62	38.6
Pond 2	8.09	<3.69	83	7	0.6	<1.00	3.09	31.1

In the last couple of years the system has gradually been expanded. The original swale ditches and banks have been increased in length and an extra one has been added. A new large pond has been excavated and added into the treatment process train. Two aerators have been fitted to this pond to compensate for not being able to make it large enough. It is no longer a fully passive system because it would have taken up too much valuable agricultural land.